

# A NEW CELL FOR ELECTROCHEMICAL CHARACTERISATION OF MANGANESE DIOXIDE FOR ALKALINE BATTERIES

V VENKATESAN AND K DAKSHINAMURTHI

Central Electrochemical Research Institute, Madras Unit, CSIR Complex, Madras 600 113, INDIA

[Received: 1991 October; Accepted: 1991 December]

A new nickel plated mild steel cell with inner dimensions of LR6 cell and with a detachable bottom plug has been designed for the evaluation of manganese dioxide particularly for alkaline cells. The technique has been standardized for rapid evaluation, by optimising graphite content, at a discharge current of  $125 \text{ mA.g}^{-1}$  simulating  $1 \Omega$  load of LR6 cell. The cell can be used for evaluation of other active materials and also for characterisation of  $\text{MnO}_2$  with respect to compactibility, conductivity, porosity, density, volume change in electrolyte and alkali absorption.

**Key words:** Manganese dioxide, alkaline batteries, electrochemical characterisation

## INTRODUCTION

Various cells [1-5] employing different conditions have been adopted for the day-to-day evaluation of manganese dioxide. Plastic cells have been predominantly used at low current drain with platinum or zinc anodes with or without reference electrodes. The graphite content in the cathode mix ranges from 3 to 10 times the weight of  $\text{MnO}_2$ . In actual practice, graphite content ranges from 0.1 to 0.15 times the weight of  $\text{MnO}_2$ . The details of the thickness, area and compaction pressures of the  $\text{MnO}_2$  cake as well as the cell design are not available in the reported cases cited. Some have used zinc gel anodes also in the cell. This paper reports electrochemical characterization studies on  $\text{MnO}_2$  that nearly simulates the conditions of LR6 cells at high discharge rate.

## EXPERIMENTAL

The details of the cell are presented in Fig. 1. The cell was nickel plated ( $2\text{--}3 \mu\text{m}$ ) including the detachable plug. The cathode mix (0.2 g electrolytic  $\text{MnO}_2$  + graphite) moistened with potassium hydroxide (1 ml of 30%) was fed into the cell and compressed at an optimised pressure [6] of  $0.6 \text{ ton.cm}^{-2}$  with a punch. Zinc gel anode (4 g) in a kuralon separator cup was used as the anode with copper lead. The cell was discharged, 15–30 minutes after fabrication, at constant current. The physical dimensions of the pellet were measured at different graphite ratios by pressing out the pellets. Electrolytic  $\text{MnO}_2$  (EMD) used in the experiments was of Indian origin. Performance of IBA 18 also was studied. As large surface area zinc powder gel anode was employed, no reference electrode was used and the potential of zinc remained nonvariant (capacity ratio  $\text{MnO}_2 : \text{Zn} = 1:52$ ). Each experiment was carried out three times per sample and reproducible results were obtained.

## RESULTS AND DISCUSSION

Features of the electrochemical cells for evaluation of  $\text{MnO}_2$  are given in Table I. A typical discharge curve for EMD sample is presented in Fig. 2. There are two discharge plateaus and the capacity calculation have been confined to cut off voltage of 1.0 V (one-electron discharge state).

### Effect of graphite content in cathode pellet

The effect of graphite addition in the cathode pellet has been studied in ratios ranging from 1 to 10 times the amount of  $\text{MnO}_2$ . The results are presented in Table II. It is seen from the discharge duration at  $125 \text{ mA.g}^{-1}$  drain that 1:1 ratio is the best. At the ratio of 1:0.1, the discharge starts at less than 1.0 V and therefore this ratio has been

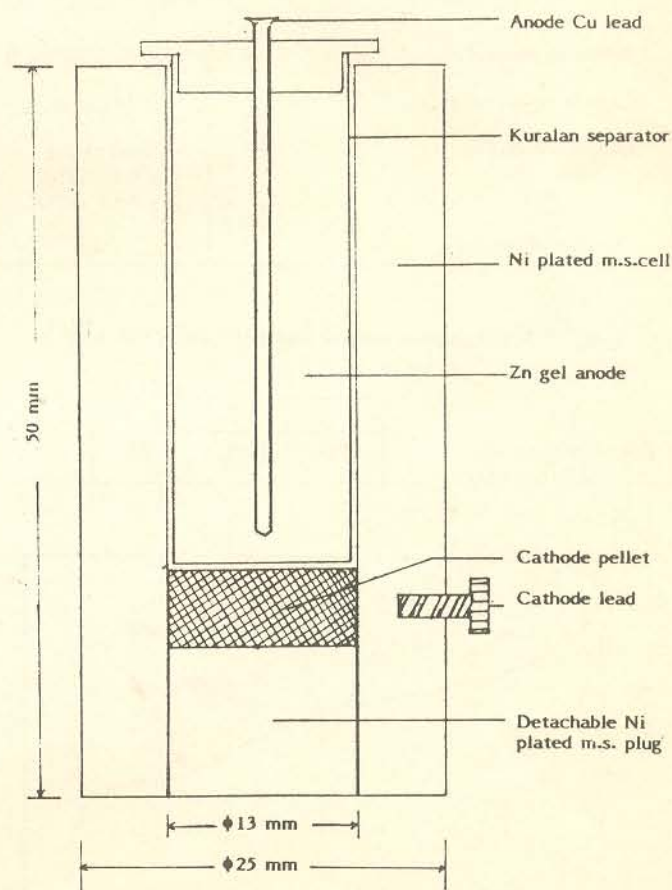


Fig. 1: Electrochemical cell for evaluation of  $\text{MnO}_2$

found to be not suitable for the studies in the cell. Therefore 1:1 ratio has been adopted for further studies.

### Effect of cathode pellet thickness

The physical dimension of the cathode pellet is presented in Table III at different graphite ratios. It is seen from the Table that at 1:1 ratio the pellet thickness is 1.80 mm which is very close to the actual cathode thickness in LR6 cell (2.20 mm). Therefore, study at this cake thickness simulates actual LR6 cell conditions. The variation of duration of discharge with pellet thickness also establishes that 1:1

TABLE-I: Features of electrochemical cells for evaluation of MnO<sub>2</sub>

1	2	3	4	5
Features	A Kozawa [1] cell	Kerr-McGee [2] (Standard test) cell	Mitsui [3] cell	CECRI cell
Cathode :				
Quantity of MnO <sub>2</sub> per expt. (g)	0.1	1	No information	0.2
MnO <sub>2</sub> : Graphite	1 : 10 (: 20) (coke)	1 : 3	"	1 : 1
Apparent area (cm <sup>2</sup> )	4.91	No information	"	1.33
Thickness (cm)	0.8	0.5	"	0.18
Pressure applied (T.cm <sup>-2</sup> )	Not defined	No information	"	0.6
Separator	Paper	Paper	Vynylon cup	Kuralon
Anode	Pt wire	Zn coil	Zn-Hg powder with Pt wire lead	Zn-Hg gel
Electrolyte	KOH (or) ZnCl <sub>2</sub> /NH <sub>4</sub> Cl	KOH	KOH	KOH
Material of construction of cell	Plastic	Plastic steel	Hard PVC with Ni rod lead	Ni plated m.s. with pull out plug
Reference electrode	Hg / HgO (or) SCE	None	None	None
Current drain (mA.g <sup>-1</sup> )	10 and 20	10 and 20	Load 10, 20 and 40 Ω	1.25
Cut off voltage (V)	- 0.20 and - 0.40 vs HgO - 0.0 V vs SCE	0.34 vs HgO (1.0 V vs Zn)	0.9	1.0 V vs Zn
Duration of test (h)	48	12	3-18	3

TABLE-II: Effect of graphite content (current drain of 125 mA.g<sup>-1</sup>)

Discharge duration upto 1.0 V (minutes)	MnO <sub>2</sub> : graphite ratio			
	1 : 1	1 : 3	1 : 5	1 : 10
	108	94	90	86

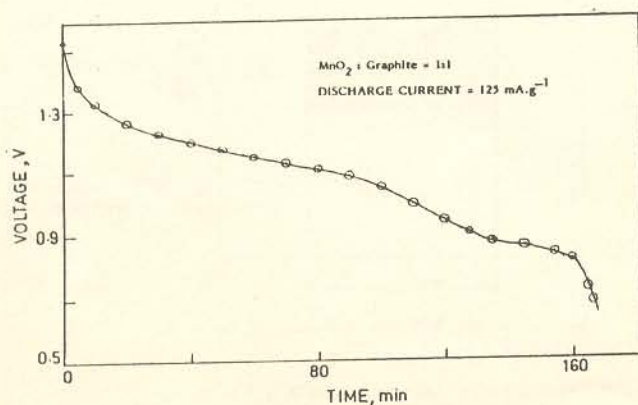


Fig. 2: Discharge curve of EMD

ratio is the best for estimating MnO<sub>2</sub> samples (Fig. 3). The apparent surface area of the cathode pellet is 1.33 cm<sup>2</sup> and is about 12% of the geometric surface area of the cathode in LR6 cell. The current drain in the test cell is therefore one order higher with respect to the apparent area in actual LR6 cell.

**Effect of current drain**

From separate discharge studies on a number of commercial LR6 cells, the average peak discharge current at 1Ω load has been found

TABLE-III: Physical dimensions of cathode pellet at different graphic additions

Pellet weight (g) Pellet thickness (mm)	MnO <sub>2</sub> : graphite ratio			
	1 : 1	1 : 3	1 : 5	1 : 10
	0.49 1.80	0.96 3.70	1.26 5.20	2.67 11.00

Pellet diameter : 1.30 cm      Pellet area : 1.33 cm<sup>2</sup>

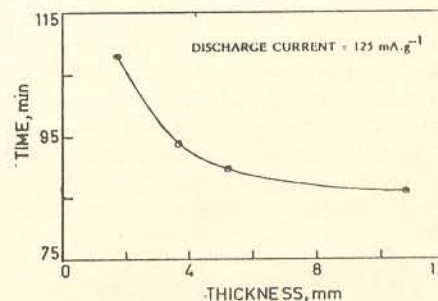


Fig. 3: Variation of duration of discharge of EMD with thickness of pellet

to be 0.95A and for a MnO<sub>2</sub> content of the cell at 7.5 g, the current drain is 125 mA.g<sup>-1</sup>. This current drain is employed for evaluation of MnO<sub>2</sub> in this paper for the rapid estimation of the electrochemical activity. However, the effect of other current drains ranging from 50 to 250 mA.g<sup>-1</sup> has been studied and their performances are presented in Table IV. It is seen that an efficiency of about 81% is achieved at 125 mA.g<sup>-1</sup> current drain for the sample employed and at lower current range. For IBA 18 sample, the discharge duration at this current drain is 120 minutes (i.e. material efficiency of 88%).

TABLE-IV: Effect of current drain ( $\text{MnO}_2$  : graphite = 1 : 1)

Cell current (mA)	Duration of discharge upto 1.0 V (minutes)	Total capacity ( $\text{mA}\cdot\text{mm}^{-1}$ )	Material efficiency* (%)
50	30	1500	45.0
25	108	2700	81.2
10	270	2700	81.2

\* For 90%  $\text{MnO}_2$  content.

### CONCLUSION

From the results presented, the best conditions for electrochemical characterisation of  $\text{MnO}_2$  for alkaline cell using the designed cell are as given in Table I (column 5). The advantages of the cell and the technique are as follows :

(i) Rapid and reproducible evaluation of  $\text{MnO}_2$  samples, (ii) High current drain simulation studies, (iii) Same cell/technique can be used for other  $\text{MnO}_2$  cells ( $\text{ZnCl}_2$  or lithium systems) or other active material with minor modifications.

Apart from electrochemical characterisation by the cell, the physical pull out of the cathode pellet facilitates the evaluation of (a) pellet density (b) porosity of pellet (c) compactability of cathode active material (d) volume changes due to alkali soak (e) electrolyte absorption and (f) conductivity of the cathode pellet.

### REFERENCES

1. A Kozawa, G Kano, K Horita and V Takeuchi, *Prog Batteries Solar Cells*, 7 (1988) 2
2. S Burkhardt and E M Spore, *ibid*, 7 (1988) 311
3. K Miyazaki and N Imada in *Proc IBA Symp (Brussels, 1983)* (Ed) A Kozawa and N Nagayama, JEC Press (1984) Ohio, p 281
4. I B Fernandes, B D Desai and V N K Dalal, *Electrochim Acta*, 29 (1984) 181
5. J Kwasinik, A Nowacki, H Purool and B Szczesniak, *Proc Symp on  $\text{MnO}_2$  electrode — Theory and Practice for Electrochemical Applications*, (Ed) B Schumm Jr., R L Middaugh, M P Grotheer and J C Hunter, *Electrochemical Society Inc, NJ USA*. (1985) p 650
6. R Illangovan, B Manivannan and K Dakshinamurthi, *Trans SAEST*, 22 (1987) 127